

# AN EXPERIMENTAL STUDY OF THE $pVTx$ PROPERTIES FOR BINARY MIXTURES OF HFC-32 AND HFC-125 IN THE RANGE OF DENSITIES FROM 900 TO 1400 $\text{kg}\cdot\text{m}^{-3}$ <sup>1</sup>

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## ABSTRACT

An experimental study of  $pVTx$  properties for binary mixtures of HFC-32( $\text{CH}_2\text{F}_2$ ) and HFC-125( $\text{C}_2\text{HF}_5$ ) was conducted in the range of temperatures from 258 to 354 K, pressures up to 16.9 MPa, densities from 900 to 1400  $\text{kg}\cdot\text{m}^{-3}$ , and compositions from 0 to 1 mol fraction of HFC-32, within the uncertainties of 4.8 mK of temperatures, 1.8 kPa of pressures, 0.022 % of densities, and 0.0022 mol fraction of compositions, respectively. The present results were measured with the use of a constant-volume apparatus consisted of the cylindrical vessel of approximately 173  $\text{cm}^3$  in its inner volume. The available data including the present measurements are critically compared with the equation of state correlated by Tillner-Roth et al. [2], and it is found that, in the liquid region for the range of compositions from 0.1 to 0.4 mol fraction of HFC-32, this equation of state [2] is not so well correlated because of the scarce experimental data.

**KEY WORDS:** experimental study; HFC-32; HFC-125; mixtures;  $pVTx$  properties

## 1. INTRODUCTION

The alternative refrigerant R410A is a mixture of 50 mass% HFC-32( $\text{CH}_2\text{F}_2$ ) and 50 mass% HFC-125( $\text{C}_2\text{HF}_5$ ) for the air-conditioning systems. However, in the condenser and evaporator of these systems, the composition of this refrigerant is changeable because of the vapor-liquid equilibrium phenomena. Therefore, the thermodynamic properties of refrigerant mixtures should be measured in the wide range of temperatures, pressures, and compositions.

This paper deals with the experimental data of pressure-volume-temperature-composition ( $pVTx$ ) properties for binary mixtures of HFC-32 and HFC-125 conducted

in the range of temperatures from 258 to 354 K, pressures from 1.6 to 16.9 MPa, densities from 900 to 1400 kg·m<sup>-3</sup>, and compositions from 0 to 1 mol fraction of HFC-32. The experimental  $pVTx$  data of this mixture have been already measured in the super-critical region for the range of compositions from 0.05 to 0.9 mol fraction of HFC-32 [1]. The available experimental data including the present measured data were compared with the equation of state correlated by Tillner-Roth et al. [2] for HFC-32, HFC-125, and their mixtures.

## 2. SURVEY OF AVAILABLE DATA OF $pVTx$ PROPERTIES

### 2.1 Pure Substances of HFC-32 and HFC-125

The  $pVT$  property data of HFC-32 have been measured, since 1993, in the range of temperatures from 142 to 424 K, pressures from 0.07 to 34.8 MPa, and densities from 2.6 to 1419 kg·m<sup>-3</sup> by Qian et al. [3], Defibaugh et al. [4], Sato et al. [5], Fu et al. [6], Fukushima et al. [7], Magee [8], and Zhang et al. [9].

The  $pVT$  property data of HFC-125 are available in the range of temperatures from 178 to 473 K, pressures from 0.1 to 35.4 MPa, and densities from 0.26 to 1683 kg·m<sup>-3</sup>, measured since 1992 by Defibaugh and Morrison [10], Baroncini et al. [11], Sagawa et al. [12], Boys Weber [13], Fukushima et al. [7], Tsvetkov et al. [14], Ye et al. [15], Magee [8], Oguchi et al. [16], and Zhang et al. [9].

### 2.2 Binary Mixtures of HFC-32 and HFC-125

The  $pVTx$  properties for binary mixtures of HFC-32 and HFC-125 are available in the range of temperatures from 200 to 440 K, pressures from 0.09 to 35.3 MPa, densities from 2.6 to 1497 kg·m<sup>-3</sup>, and compositions from 0.05 to 0.9 mol fraction of HFC-32. Widiatmo et al. [17] measured 24 data points in the range of temperatures from 280 to 310 K, pressures from 0.88 to 2.3 MPa, densities from 940 to 1254 kg·m<sup>-3</sup>, and compositions from 0.2 to 0.9 mol fraction of HFC-32. Weber et al. [18] measured 17 data points in the range of temperatures from 338 to 373 K, pressures from 0.3 to 4.2 MPa, densities from 8.8 to 158.1 kg·m<sup>-3</sup>, and compositions at 0.5 mol fraction of HFC-32. Bivence et al. [19] also measured 111 data points in the range of temperatures from 280 to 373 K, pressures from 0.49 to 4.8 MPa, densities from 13.7 to 206 kg·m<sup>-3</sup>, and compositions from 0.65 to 0.78 mol fraction of HFC-32. Zhelezny et al. [20] obtained 136 data points in the range of temperatures from 280 to 338 K, pressures from 0.67 to 3.6 MPa, densities from 20 to 184 kg·m<sup>-3</sup>, and compositions from 0.26 to 0.75 mol fraction of HFC-32. Kiyoura et al. [21] obtained 104 data points in the range of temperatures from 320 to 440 K, pressures from 1.7 to 5.2 MPa, densities from 67.7 to 158 kg·m<sup>-3</sup>, and compositions from 0.37 to 0.61 mol fraction of HFC-32. Sato et al. [22] also obtained 156 data points in the range of temperatures from 320 to 440 K, pressures

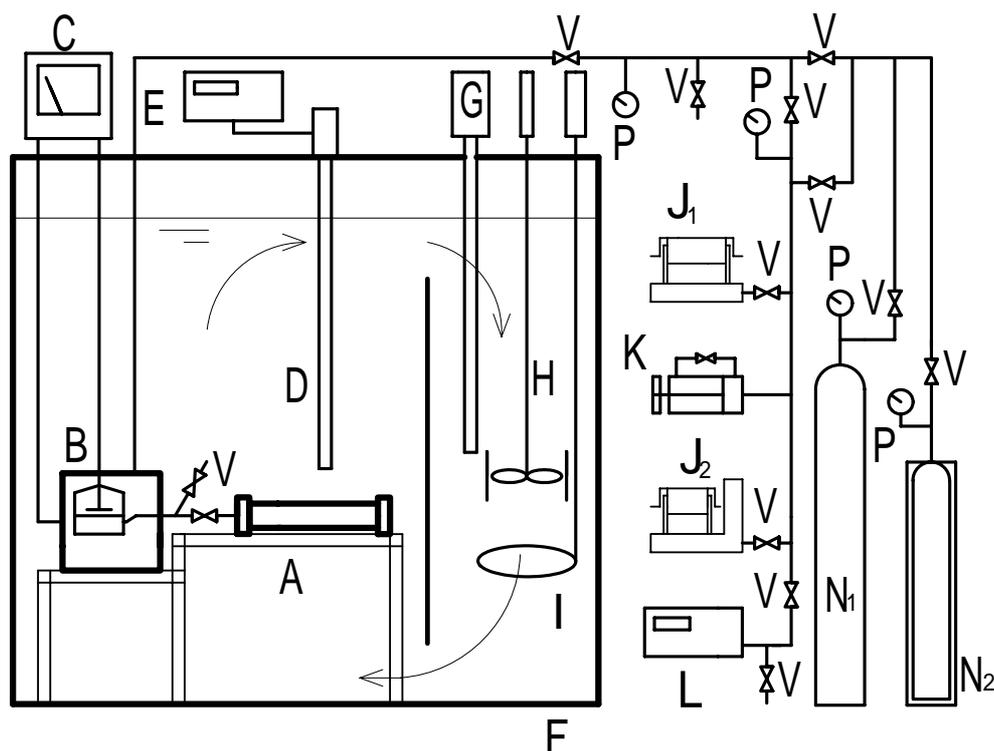
from 1.72 to 5.3 MPa, densities from 50.4 to 125.1 kg·m<sup>-3</sup>, and compositions from 0.70 to 0.90 mol fraction of HFC-32. Zhang et al.[9] reported 124 data points in the range of temperatures from 300 to 380 K, pressures from 0.09 to 4.6 MPa, densities from 2.6 to 151.7 kg·m<sup>-3</sup>, and compositions from 0.50 to 0.70 mol fraction of HFC-32. Magee and Haynes [23] reported 228 data points in the range of temperatures from 200 to 399 K, pressures from 4.27 to 35.3 MPa, densities from 91.5 to 1497 kg·m<sup>-3</sup>, and compositions at 0.5 mol fraction of HFC-32. Miyazaki et al.[2] also reported 79 data points in the range of temperatures from 343 to 423 K, pressures from 4.0 to 15.6 MPa, densities from 485 to 491 kg·m<sup>-3</sup>, and compositions from 0.05 to 0.90 mol fraction of HFC-32. Most  $pVTx$  property data of binary mixtures of HFC-32 and HFC-125 have been measured in the range of temperatures above 300 K and densities below 200 kg·m<sup>-3</sup>.

### 3. METHOD AND UNCERTAINTIES

A constant-volume apparatus with a cylindrical vessel of approximately 173 cm<sup>3</sup> in its inner volume was used for the present measurements of  $pVTx$  properties, as shown in Fig.1.

The sample of the binary mixture of HFC-32 and HFC-125 was prepared as follows: After having weighed precisely each mass of the piezometer, namely cylindrical vessel, and the sample supplier in vacuum, HFC-32 was charged into the sample supplier and HFC-125 also charged into the piezometer while controlling the mass of each charged sample, respectively: Both the sample supplier with HFC-32 and the piezometer with HFC-125 were weighed carefully and precisely by the balance: Then, HFC-32 in the sample supplier was additionally charged into the piezometer of HFC-125 frozen by liquid nitrogen, and finally the mass of the mixture of HFC-32 and HFC-125 was weighed precisely by the balance.

This experimental method was described in other literatures[1, 16, 24, 25]. Normally, density and composition distributions caused by gravity effect in the vessel exist. For making less effect for the  $pVTx$  measurements, in this present study was used of a low-height cylindrical vessel. Temperature was measured with the use of a platinum resistance thermometer calibrated within 2 mK at the National Physical Laboratory in United Kingdom, based on the International Temperature Scale (1990). The RUSKA series 6000 of a quartz Bourdon type pressure gage was used for the measurements of pressures. Density was determined by means of a mass of the sample divided by an inner volume of the vessel. Composition was calculated with aid of each mass of the sample of HFC-32 and HFC-125. Uncertainties of the present data were within 4.8 mK of temperature, 1.8 kPa of pressure, 0.022 % of density, and 0.0022 mol fraction, respectively. The purities of the samples of HFC-32 and HFC-125 were 0.99983 and 0.9983 mol fraction, respectively.



- |   |   |
|---|---|
| A: Piezometer                               | I: Heater                                   |
| B: Diaphragm type pressure balance detector | J <sub>1,2</sub> : Air piston pressure gage |
| C: Transformer bridge                       | K: Pressure controller                      |
| D: Platinum resistance thermometer          | L: Digital pressure gage                    |
| E: Thermometer bridge                       | N <sub>1,2</sub> : Nitrogen bottle          |
| F: Thermostated bath                        | P: Bourdon type pressure gages              |
| G: Cooler                                   | V: High pressure valves                     |
| H: Circular pump                            | ←: Flow pattern of brine                    |

Fig. 1. Schematic diagram of the  $pVTx$  apparatus.

#### 4. RESULTS

Thermodynamic properties for the refrigerators and air-conditioning machines are required in the range of temperatures below 273 K, but most available data for binary mixtures of HFC-32 and HFC-125 have been measured in the vapor region for the range of temperatures above 300 K. Therefore, the present experimental works were focused on the low temperature liquid region.

The 102 data points of  $pVTx$  properties for binary mixtures of HFC-32 and HFC-125 were measured in the range of temperatures from 258 to 354 K, pressures from 1.6 to 16.9 MPa, densities from 900 to 1400 kg·m<sup>-3</sup>, and compositions from 0 to 1 mol fraction of HFC-32, as shown in Tab. I.

Table I. Experimental Results for  $pVTx$  Properties for Binary Mixtures of HFC-32 and HFC-125

| Mol fraction of HFC-32 | Temperature (K) | Pressure (MPa) | Density ( $\text{kg}\cdot\text{m}^{-3}$ ) |
|------------------------|-----------------|----------------|---|
| 0.0000                 | 258.157         | 4.5956         | 1403.78                                   |
| 0.0000                 | 261.154         | 6.5798         | 1403.47                                   |
| 0.0000                 | 262.143         | 7.2846         | 1403.36                                   |
| 0.0000                 | 267.159         | 10.8092        | 1402.84                                   |
| 0.0000                 | 270.192         | 13.0028        | 1402.53                                   |
| 0.0000                 | 273.152         | 15.0759        | 1402.23                                   |
| 0.0000                 | 275.154         | 16.5720        | 1402.04                                   |
| 0.0980                 | 264.148         | 3.2352         | 1362.36                                   |
| 0.0980                 | 267.160         | 5.3013         | 1362.04                                   |
| 0.0980                 | 270.153         | 7.4144         | 1361.73                                   |
| 0.0980                 | 273.151         | 9.5327         | 1361.42                                   |
| 0.0980                 | 282.151         | 15.9775        | 1360.53                                   |
| 0.1000                 | 313.146         | 2.8206         | 1097.54                                   |
| 0.1000                 | 318.151         | 4.5285         | 1097.17                                   |
| 0.1000                 | 323.159         | 6.2529         | 1096.79                                   |
| 0.1000                 | 328.146         | 7.9860         | 1096.43                                   |
| 0.1000                 | 333.168         | 9.7419         | 1096.06                                   |
| 0.1000                 | 338.144         | 11.4891        | 1095.70                                   |
| 0.1000                 | 343.127         | 13.2472        | 1095.35                                   |
| 0.1000                 | 348.161         | 15.0221        | 1094.99                                   |
| 0.1000                 | 353.138         | 16.7818        | 1094.64                                   |
| 0.3004                 | 258.149         | 2.1770         | 1342.88                                   |
| 0.3004                 | 259.150         | 2.9131         | 1342.77                                   |
| 0.3004                 | 261.150         | 4.4749         | 1342.56                                   |
| 0.3004                 | 263.153         | 6.1063         | 1342.34                                   |
| 0.3004                 | 265.146         | 7.7670         | 1342.13                                   |
| 0.3004                 | 267.158         | 9.3829         | 1341.92                                   |
| 0.3004                 | 269.150         | 10.9833        | 1341.71                                   |

Table I. (Continued)

| Mol fraction<br>of HFC-32 | Temperature<br>(K) | Pressure<br>(MPa) | Density<br>(kg·m <sup>-3</sup> ) |
|---------------------------|--------------------|-------------------|----------------------------------|
| 0.3004                    | 273.148            | 14.2551           | 1341.32                          |
| 0.3003                    | 313.134            | 2.2175            | 1050.39                          |
| 0.3003                    | 318.183            | 3.9013            | 1050.03                          |
| 0.3003                    | 323.160            | 5.6459            | 1049.68                          |
| 0.3003                    | 328.150            | 7.4089            | 1049.33                          |
| 0.3003                    | 333.142            | 9.1884            | 1048.98                          |
| 0.3003                    | 338.134            | 10.9786           | 1048.63                          |
| 0.3003                    | 343.127            | 12.7725           | 1048.29                          |
| 0.3003                    | 348.168            | 14.5923           | 1047.95                          |
| 0.3003                    | 353.136            | 16.3860           | 1047.61                          |
| 0.3003                    | 354.135            | 16.7440           | 1047.54                          |
| 0.4995                    | 258.157            | 1.5544            | 1294.18                          |
| 0.4995                    | 259.150            | 2.4037            | 1294.07                          |
| 0.4995                    | 261.150            | 4.1183            | 1293.85                          |
| 0.4995                    | 263.147            | 5.8485            | 1293.64                          |
| 0.4995                    | 265.167            | 7.5859            | 1293.43                          |
| 0.4995                    | 267.146            | 9.2744            | 1293.23                          |
| 0.4995                    | 268.197            | 10.1515           | 1293.13                          |
| 0.4995                    | 269.138            | 10.9505           | 1293.04                          |
| 0.4995                    | 271.135            | 12.6474           | 1292.84                          |
| 0.4995                    | 273.080            | 14.3114           | 1292.65                          |
| 0.4995                    | 275.133            | 16.0655           | 1292.46                          |
| 0.4993                    | 318.207            | 3.3418            | 1000.30                          |
| 0.4993                    | 323.150            | 5.1293            | 999.96                           |
| 0.4993                    | 328.163            | 6.9697            | 999.62                           |
| 0.4993                    | 333.154            | 8.8145            | 999.29                           |
| 0.4993                    | 338.191            | 10.6899           | 998.95                           |
| 0.4993                    | 343.183            | 12.5499           | 998.62                           |
| 0.4993                    | 348.164            | 14.4227           | 998.30                           |
| 0.4993                    | 353.128            | 16.2902           | 997.98                           |

Table I. (Continued)

| Mol fraction<br>of HFC-32 | Temperature<br>(K) | Pressure<br>(MPa) | Density<br>(kg·m <sup>-3</sup> ) |
|---------------------------|--------------------|-------------------|----------------------------------|
| 0.4993                    | 354.148            | 16.6721           | 997.91                           |
| 0.6995                    | 259.140            | 2.6583            | 1234.39                          |
| 0.6995                    | 261.150            | 4.5162            | 1234.17                          |
| 0.6995                    | 263.150            | 6.3629            | 1233.97                          |
| 0.6995                    | 264.151            | 7.2881            | 1233.88                          |
| 0.6995                    | 265.154            | 8.2136            | 1233.78                          |
| 0.6995                    | 267.147            | 10.0512           | 1233.58                          |
| 0.6995                    | 269.151            | 11.8944           | 1233.38                          |
| 0.6995                    | 271.156            | 13.7402           | 1233.20                          |
| 0.6995                    | 273.159            | 15.5793           | 1233.01                          |
| 0.6995                    | 274.162            | 16.4994           | 1232.92                          |
| 0.6998                    | 318.150            | 2.9218            | 949.66                           |
| 0.6998                    | 323.144            | 4.8670            | 949.34                           |
| 0.6998                    | 328.137            | 6.8399            | 949.01                           |
| 0.6998                    | 333.127            | 8.8340            | 948.69                           |
| 0.6998                    | 338.126            | 10.8431           | 948.37                           |
| 0.6998                    | 343.121            | 12.8603           | 948.05                           |
| 0.6998                    | 348.123            | 14.8870           | 947.74                           |
| 0.6998                    | 353.108            | 16.9168           | 947.43                           |
| 0.8992                    | 318.145            | 2.9590            | 900.95                           |
| 0.8992                    | 323.129            | 5.2123            | 900.63                           |
| 0.8992                    | 328.160            | 7.5092            | 900.31                           |
| 0.8992                    | 333.130            | 9.7934            | 900.01                           |
| 0.8992                    | 338.123            | 12.1003           | 899.70                           |
| 0.8992                    | 343.120            | 14.4191           | 899.40                           |
| 0.8992                    | 348.126            | 16.7457           | 899.10                           |
| 0.8997                    | 261.147            | 3.0611            | 1151.87                          |
| 0.8997                    | 262.144            | 4.0560            | 1151.77                          |
| 0.8997                    | 263.150            | 5.0583            | 1151.67                          |
| 0.8997                    | 264.150            | 6.0535            | 1151.57                          |

Table I. (Continued)

| Mol fraction<br>of HFC-32 | Temperature<br>(K) | Pressure<br>(MPa) | Density<br>(kg·m <sup>-3</sup> ) |
|---------------------------|--------------------|-------------------|----------------------------------|
| 0.8997                    | 265.153            | 7.0509            | 1151.47                          |
| 0.8997                    | 267.153            | 9.0409            | 1151.28                          |
| 0.8997                    | 268.151            | 10.0319           | 1151.19                          |
| 0.8997                    | 269.158            | 11.0311           | 1151.09                          |
| 0.8997                    | 271.151            | 13.0075           | 1150.92                          |
| 0.8997                    | 273.155            | 14.9905           | 1150.74                          |
| 0.8997                    | 274.145            | 15.9693           | 1150.66                          |
| 1.0000                    | 313.158            | 3.3537            | 900.17                           |
| 1.0000                    | 316.153            | 4.9671            | 899.97                           |
| 1.0000                    | 319.149            | 6.5714            | 899.77                           |
| 1.0000                    | 322.151            | 8.1624            | 899.57                           |
| 1.0000                    | 328.156            | 11.3997           | 899.19                           |
| 1.0000                    | 334.149            | 14.7534           | 898.82                           |
| 1.0000                    | 337.153            | 16.5805           | 898.63                           |

## 5. DISCUSSION

### 5.1 Pure Substances of HFC-32 and HFC-125

The deviations of available measured densities of HFC-32 from the equation of state [2] are shown in Fig.2 for the range of densities from 648 to 1420 kg·m<sup>-3</sup> [4, 5, 7, 8].

The data by Fukushima et al. [7] are plotted in Fig. 2 around the deviation of 0.36 to 4.6 % in density deviation from the equation of state [2], and the other data including the present data sets are distributed within  $\pm 0.2$  %

The deviations of available observed densities of HFC-125 from the equation of state [2] are shown in Fig.3 for the range of densities from 817 to 1684 kg·m<sup>-3</sup> [7, 8, 10, 12, 16]. The data by Sagawa et al. [12] are plotted in Fig. 3 around the density deviation of -0.94 to -0.05 %, and the data by Oguchi et al. [16] are located around the deviation of 0.33 to 0.60 % in density deviation. The other data including the present data sets are distributed within  $\pm 0.2$  % in density, as shown in Fig. 3.

## 5.2 Binary Mixtures of HFC-32 and HFC-125

The deviations of available measured densities for binary mixtures of HFC-32 and HFC-125 from the equation of state [2] are shown in Fig. 4 for the range of densities from 898 to 1255 kg·m<sup>-3</sup> [17, 23].

The data by Widiatmo et al. [17] are plotted in Fig. 4 around the density deviation of -0.23 to 0.61 %, the data by Magee and Haynes [23] around the density deviation of -0.07 to 0.21 %, and the present data around the density deviation of -0.22 to 0.59 %. In the range of compositions from 0.5 to 0.9 mol fraction of HFC-32, the density deviation of the available data including the present data are distributed from -0.2 to 0.4 %, but in the range of compositions from 0.1 to 0.4 mol fraction of HFC-32, the data by Widiatmo et al. [17] and the present data were located around the deviation of 0.2 to 0.6 %.

The density deviations from the equation of state [2] are shown in Fig. 5 for the range of densities from 1150 to 1397 kg·m<sup>-3</sup> [23] of the binary mixtures of HFC-32 and HFC-125.

The present data are located in Fig.5 around the density deviation of 0.14 to 0.41 %, and the data by Magee and Haynes [23] around the density deviation of 0.10 to 0.19 %.

In the range of densities from 888 to 1255 kg·m<sup>-3</sup>, the present data agree with the data by Magee and Haynes [23] within  $\pm 0.1$  % in density.

In the vapor region and super-critical region, pressure deviations of the most available data from the equation of state [2] are distributed within  $\pm 0.5$  % in pressure.

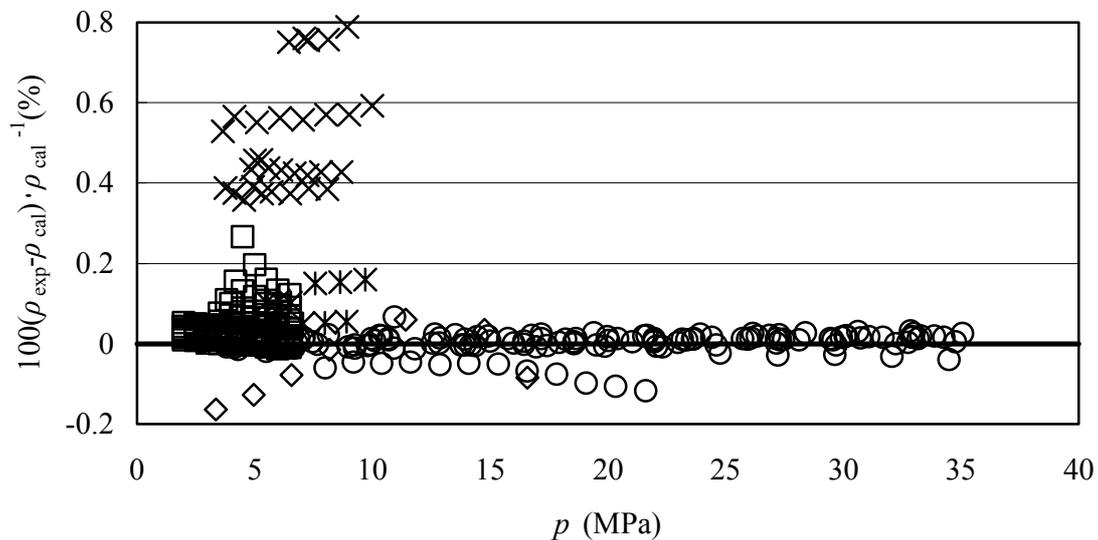


Fig. 2. Density deviations of the present results and available  $pVT$  properties of HFC-32 from the equation of state [2]. (Densities from 649 to 1420 kg·m<sup>-3</sup>). (□) Defibaugh et al. [4]: =737.44 to 1157.22 kg·m<sup>-3</sup>. (\*) Sato et al. [5]: =673.90 to 850.15 kg·m<sup>-3</sup>. (×) Fukushima et al. [7]: =648.7 to 802.7 kg·m<sup>-3</sup>. (○) Magee et al. [8]: =708.00 to 1419.50 kg·m<sup>-3</sup>. (◇) This work: =899.34 to 901.64 kg·m<sup>-3</sup>.

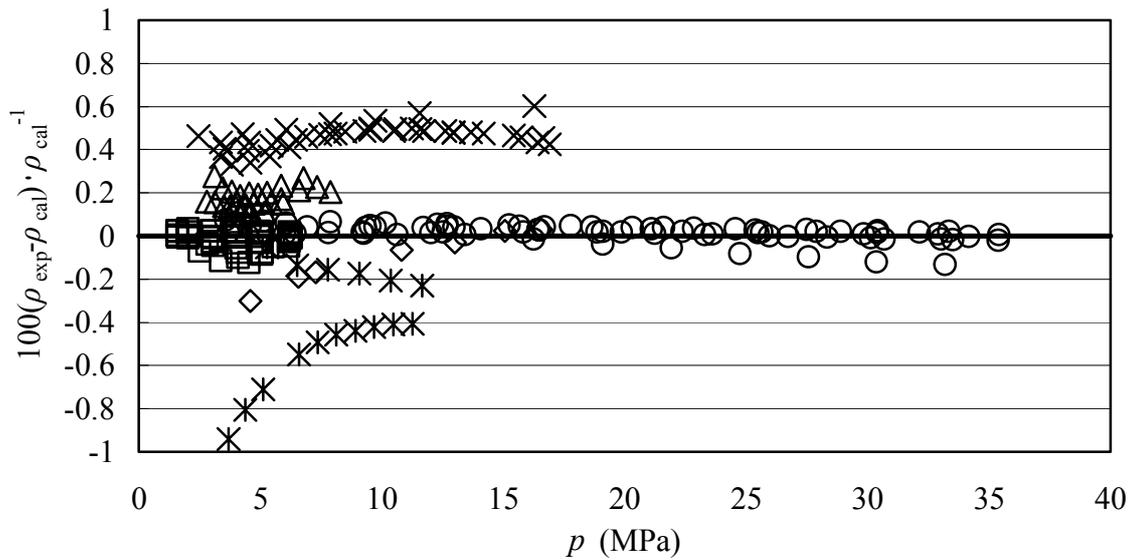


Fig. 3. Density deviations of the present results and available  $pVT$  properties of HFC-125 from the equation of state [2]. (Densities from 734 to 1684  $\text{kg}\cdot\text{m}^{-3}$ ). ( $\triangle$ ) Fukushima et al. [7]: =804.8 to 997.4  $\text{kg}\cdot\text{m}^{-3}$ . ( $\square$ ) Defibaugh and Morrison [10]: =817.90 to 1348.40  $\text{kg}\cdot\text{m}^{-3}$ . ( $*$ ) Sagawa et al. [12]: =734.37 to 940.01  $\text{kg}\cdot\text{m}^{-3}$ . ( $\circ$ ) Magee et al. [8]: =1114.60 to 1683.70  $\text{kg}\cdot\text{m}^{-3}$ . ( $\times$ ) Oguchi et al. [16]: =845.08 to 1145.32  $\text{kg}\cdot\text{m}^{-3}$ . ( $\diamond$ ) This work: =1402.04 to 1403.78  $\text{kg}\cdot\text{m}^{-3}$ .

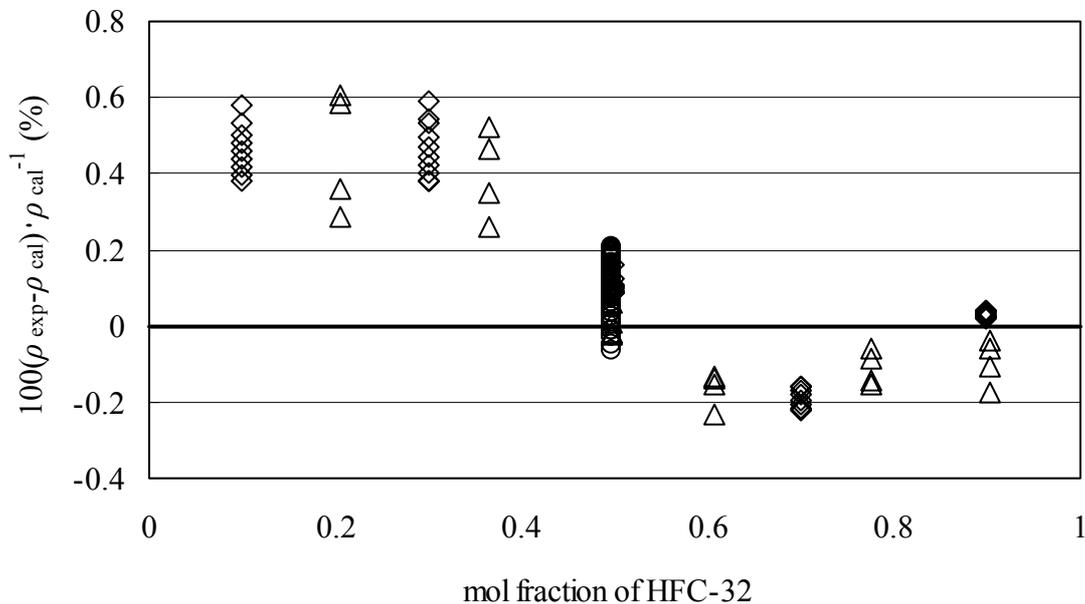


Fig. 4. Density deviations of the data by Widiatmo et al. [17], Magee and Haynes [23] and the present results from the equation of state [2] for binary mixtures of HFC-32 and HFC-125 (Densities from 898 to 1255  $\text{kg}\cdot\text{m}^{-3}$ ). ( $\triangle$ ) Widiatmo et al. [17]: =940.5 to 1254.6  $\text{kg}\cdot\text{m}^{-3}$ . ( $\circ$ ) Magee and Haynes [23]: =888.12. to 1033.11  $\text{kg}\cdot\text{m}^{-3}$ . ( $\diamond$ ) This work: =898.71 to 1091.20  $\text{kg}\cdot\text{m}^{-3}$ .

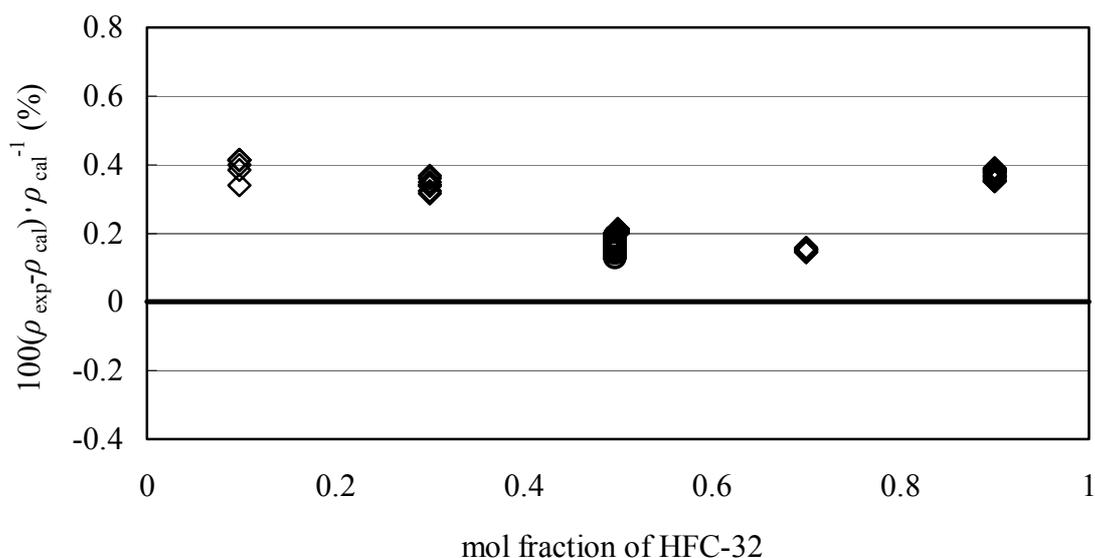


Fig. 5. Density deviations of the data by Magee and Haynes [23] and the present results from the equation of state [2] for binary mixtures of HFC-32 and HFC-125. (Densities from 1150 to 1363 kg·m<sup>-3</sup>). (○) Magee and Haynes [23]: =940.5 to 1254.6 kg·m<sup>-3</sup>. (◇) This work: =1270.99 to 1334.96 kg·m<sup>-3</sup>.

## 6. CONCLUSION

The 102 data points of  $pVTx$  properties for binary mixtures of HFC-32 and HFC-125 were measured with the use of a constant-volume apparatus in the range of temperatures from 258 to 354 K, pressures from 1.6 to 16.9 MPa, densities from 900 to 1400 kg·m<sup>-3</sup>, and compositions from 0 to 1 mol fraction of HFC-32, as shown in Tab. I. The available data of this mixture are compared with the equation of state [2] as shown in Fig. 2 to 5, and it is found that, in the liquid region for the range of compositions from 0.1 to 0.4 mol fraction of HFC-32, the equation of state [2] is not so well correlated because of scarce experimental data.

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